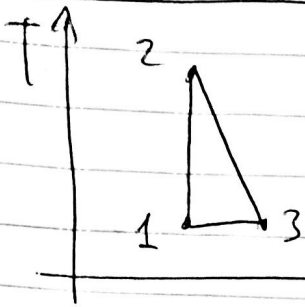


SOLUZIONI ESAME TERMODINAMICA FEBBRAIO 2024

1



$$\frac{T_2}{T_1} = \frac{T_2}{T_3} = 3$$

$$\frac{S_3}{S_1} = \frac{S_3}{S_2} = 2$$

Calcoliamo $Q, W, \Delta U$ valore per valore

1 → 2

$$Q_{12} = \int_1^2 T dS = 0$$

$$\Delta U = Q - W$$

$$\Delta U_{12} = n c_v \Delta T = \frac{5}{2} n R (3T_1 - T_1) = + 5 n R T_1$$

$$W_{12} = Q_{12} - \Delta U_{12} = -5 n R T_1$$

2 → 3

$$Q_{23} = \text{area trapezoido} = \frac{(T_2 + T_1)(S_3 - S_1)}{2} = \frac{4T_1 S_1}{2} = 2T_1 S_1$$

$$Q_{23} > 0 \rightarrow Q_{in}$$

$$\Delta U_{23} = n c_v \Delta T = \frac{5}{2} n R (T_1 - 3T_1) = -5 n R T_1$$

$$W_{23} = Q_{23} - \Delta U_{23} = 2T_1 S_1 + 5 n R T_1$$

3 → 1

$$Q_{31} = \int_3^1 T dS = T_1 (S_1 - S_3) = T_1 (S_1 - 2S_1) = -T_1 S_1$$

$$Q_{31} < 0 \Rightarrow Q_{out}$$

$$\Delta U_{31} = n c_v \Delta T = 0$$

$$W_{31} = Q_{31} - \Delta U_{31} = -T_1 S_1$$

$$Q_{tot} = T_1 S_1 \quad W_{tot} = T_1 S_1 \quad \rightarrow \Delta U_{tot} = 0 \quad \checkmark$$

$$Q_{in} = 2T_1 S_1 \quad Q_{out} = -T_1 S_1$$

$$a) \quad \eta = \frac{W_{tot}}{Q_{in}} = \frac{T_1 S_1}{2T_1 S_1} = \frac{1}{2} \quad \circ \quad \eta = 1 - \frac{|Q_{out}|}{Q_{in}} = 1 - \frac{T_1 S_1}{2T_1 S_1} = 1 - \frac{1}{2} = \frac{1}{2}$$

$$b) \quad \eta_{Carnot} = 1 - \frac{T_{min}}{T_{max}} = 1 - \frac{T_1}{T_2} = 1 - \frac{T_1}{3T_1} = 1 - \frac{1}{3} = \frac{2}{3} \quad \frac{1}{2} < \frac{2}{3}$$

c) Siccome tutti i rami sono reversibili, $\Delta S_{amb} = -\Delta S_{gas}$

$$1 \rightarrow 2 \quad \Delta S_{gas} = 0 \rightarrow \Delta S_{amb} = 0$$

$$2 \rightarrow 3 \quad \Delta S_{gas} = +S_1 \rightarrow \Delta S_{amb} = -S_1$$

$$3 \rightarrow 1 \quad \Delta S_{gas} = -S_1 \rightarrow \Delta S_{amb} = +S_1$$

d) È banalmente 0 in quanto l'ambiente circostante è considerato per definizione non partecipa alle trasformazioni

e) non cambierebbe niente in quanto W_{tot}, Q_{in}, Q_{out} non cambiano. W sui singoli rami dipende da $C_v (= \frac{3}{2}R \text{ o } \frac{5}{2}R)$ ma W_{tot} no!

$$f) \quad \begin{array}{c} \uparrow \\ \text{2} \\ \text{1} \text{-----} \text{3} \\ \downarrow \end{array} \quad \Rightarrow \quad \Delta S_{gas} = nR \frac{dT}{T} + nR \frac{dV}{V} = nR \frac{dV}{V} \quad T = \text{const}$$

$$\Rightarrow \Delta S_{gas} = S_1 - S_3 = -S_1$$

$$\Delta S_{gas} = \int dS_{gas} = \int nR \frac{dV}{V} = nR \ln \left(\frac{V_1}{V_3} \right)$$

$$\Rightarrow nR \ln \left(\frac{V_1}{V_3} \right) = -S_1 < 0 \rightarrow \ln \left(\frac{V_1}{V_3} \right) < 0 \rightarrow V_1 < V_3$$

quindi il gas si contrae

$$nR \ln \left(\frac{V_1}{V_3} \right) = -S_1 \rightarrow \frac{V_1}{V_3} = e^{-\frac{S_1}{nR}}$$

$$T = \text{const} \Rightarrow PV = \text{const} \Rightarrow \frac{P_1 V_1}{P_3 V_3} = \text{const} \Rightarrow \frac{P_1}{P_3} = \frac{V_3}{V_1} = e^{\frac{S_1}{nR}}$$

[2]

a) $T(V) = \alpha V$ $V_i \rightarrow V_f = \beta V_i$

$$T_i = \alpha V_i \rightarrow T_f = \alpha V_f = \alpha \beta V_i = \beta T_i$$

$$PV = nRT \rightarrow P = \frac{nRT}{V} = \frac{nR\alpha V}{V} = nR\alpha = \text{const}$$

$$W = \int dV P(V) = nR\alpha \int dV = nR\alpha (V_f - V_i) =$$

$$= nR\alpha (\beta V_i - V_i) = nR\alpha (\beta - 1) V_i = nR\alpha (\beta - 1) \frac{T_i}{\alpha} = nR(\beta - 1) T_i$$

$$\Delta U = nC_V \Delta T = \frac{5}{2} nR (T_f - T_i) = \frac{5}{2} nR (\beta - 1) T_i$$

$$Q = \Delta U + W = nR(\beta - 1) T_i + \frac{5}{2} nR (\beta - 1) T_i = \frac{7}{2} nR (\beta - 1) T_i$$

b) $T(P) = \alpha P$ $P_i \rightarrow P_f = \beta P_i$

$$T_i \rightarrow T_f = \beta T_i \quad \text{come sopra}$$

$$PV = nRT \rightarrow V = \frac{nRT}{P} = \frac{nR\alpha P}{P} = nR\alpha = \text{const}$$

$$W = \int dV P(V) = 0$$

$$\Delta U = nC_V \Delta T = \frac{5}{2} nR (T_f - T_i) = \frac{5}{2} nR (\beta - 1) T_i$$

$$Q = \Delta U + W = \frac{5}{2} nR (\beta - 1) T_i$$

c) $T(S) = \alpha S$

$$S_i \rightarrow S_f = \beta S_i$$

$$T_i \rightarrow T_f = \beta T_i \quad \text{come sopra}$$

$$Q = \int dS T(S) = \int_{S_i}^{S_f} dS \alpha S = \alpha \frac{S^2}{2} \Big|_{S_i}^{S_f} = \frac{\alpha}{2} (S_f^2 - S_i^2) =$$

$$= \frac{\alpha}{2} (\beta^2 S_i^2 - S_i^2) = \frac{\alpha}{2} (\beta^2 - 1) S_i^2 = \frac{\alpha}{2} (\beta^2 - 1) \frac{T_i^2}{\alpha^2} = \frac{(\beta^2 - 1)}{2\alpha} T_i^2$$

$$\Delta U = n c_v \Delta T = \frac{5}{2} n R (T_f - T_i) = \frac{5}{2} n R (\beta - 1) T_i$$

$$W = Q - \Delta U = \frac{\beta^2 - 1}{2\alpha} T_i^2 - \frac{5}{2} n R (\beta - 1) T_i$$

Per quant riguarda ΔS_{amb} , questa è $\Delta S_{\text{amb}} = -\Delta S_{\text{gas}}$ per tutte e tre i casi essendo le trasformazioni reversibili

$$\begin{aligned} a) \Delta S_{\text{gas}} &= \int dS_{\text{gas}} = \int n c_v \frac{dT}{T} + \int n R \frac{dV}{V} = n c_v \ln\left(\frac{T_f}{T_i}\right) + n R \ln\left(\frac{V_f}{V_i}\right) \\ &= n c_v \ln \beta + n R \ln \beta = \frac{7}{2} n R \ln \beta \end{aligned}$$

$$\Rightarrow \Delta S_{\text{amb}} = -\frac{7}{2} n R \ln \beta \quad V_i = V_f$$

$$\begin{aligned} b) \Delta S_{\text{gas}} &= n c_v \ln\left(\frac{T_f}{T_i}\right) + n R \ln\left(\frac{V_f}{V_i}\right) = n c_v \ln \beta = \frac{5}{2} n R \ln \beta \\ \Delta S_{\text{amb}} &= -\frac{5}{2} n R \ln \beta \end{aligned}$$

$$c) \text{Banalmente } \Delta S_{\text{gas}} = S_f - S_i = \frac{5}{2} n R (\beta - 1) S_i \Rightarrow \Delta S_{\text{amb}} = -(1-\beta) S_i$$

3

~~$P = 100 \text{ W}$~~ ~~$P = 100 \text{ J}$~~ ~~$V = 8 \text{ m}^3$~~ ~~$c_v = \frac{5}{2} R$~~

Panetti rigide \rightarrow trasformazione \sim isocora (non adiabatica perché c'è scambio di calore con l'aria \leftrightarrow universo)

$$T_i = 20^\circ\text{C} = 293.15 \text{ K}$$

$$T_f = 55^\circ\text{C} = 328.15 \text{ K}$$

$$P_i = P_{\text{atm}} \sim 1.01325 \times 10^5 \text{ Pa}$$

$$P (= 100 \text{ W} \quad \text{o} \quad 1000 \text{ W})$$

$$N (= 100 \quad \text{o} \quad 30)$$

$$V = 8 \text{ m}^3 \sim (20 \times 20 \times 3) \text{ m}^3$$

$$Q = N P \Delta t = \frac{5}{2} n R \Delta T \Rightarrow \Delta t = \frac{5 n R \Delta T}{2 N P}$$

ma $\frac{P V}{T_i} = n R T_i \rightarrow n = \frac{P_i V}{R T_i}$

$$\Delta t = \frac{5 n R \Delta T}{2 N P} = \frac{5 P_i V R \Delta T}{2 R T_i N P} = \frac{5 P_i V \Delta T}{2 T_i N P} =$$

$$= \frac{5 P_i x y z (T_f - T_i)}{2 T_i N P}$$

Controllo unità

$$[] = \frac{\text{Pa} \cdot \text{m} \cdot \text{m} \cdot \text{m} \cdot \text{K}}{\text{K} \cdot \text{W}} = \frac{\frac{\text{kg}}{\text{m} \cdot \text{s}^2} \cdot \text{m}^3 \cdot \text{K}}{\text{K} \cdot \frac{\text{kg} \cdot \text{m}}{\text{s}^2}} = \text{s}$$

Quindi $\Delta t = \frac{5 P_i x y z (T_f - T_i)}{2 T_i N P}$ in s

a) Mettendo i numeri viene $\Delta t = 3629.4 \text{ s} \sim 61 \text{ min}$
 Quindi muovono alle 21:01

b) $\Delta t = 12097.5 \text{ s} \sim 202 \text{ min} = 3 \text{ hr } 22 \text{ min}$
 Quindi muovono alle 23:22

c) $\Delta t = 362.92 \text{ s} \sim 6 \text{ min}$
 Quindi muovono alle 20:06

d) Ovviamente $\Delta U_{\text{tot}} = 0$ perché $Q_{\text{tot}} = 0$ (processo adiabatico) e $W_{\text{tot}} = 0$ (parti rigide), il calore scambiato solo internamente al sistema

e) L'ambiente esterno avrebbe rallezato il riscaldamento (ammendo che fuori facesse <55°C!)